

A Total Cost of Ownership Model for Design and Manufacturing Optimization of Fuel Cells in Stationary and Emerging Market Applications

Department of Energy Annual Merit Review for Fuel Cell Research

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Project ID # FC098

This presentation does not contain any proprietary, confidential, or otherwise restricted information

Overview AMR 2014



Timeline

Project start date: Oct 2011

Project end date: Sept 2016

Percent complete: 60%

Budget

Total project funding

DOE share: \$1.9M

Contractor share: n.a.

FY13 DOE Funding: \$600k

Planned Funding for FY14: \$374k

DOE Cost Targets

Characteristic	2015 Target	2020 Target
10kW CHP System	\$1900/kW	\$1700/kW
100kW CHP System	\$2300/kW	\$1000/kW

Barriers Addressed

- Fuel-cell cost: expansion of cost envelope to total cost of ownership including full life cycle costs and externalities (MYPP 3.4.5B)
- Lack of High-Volume Membrane Electrode Assembly Processes (MYPP 3.5.5A)
- Lack of High-Speed Bipolar Plate Manufacturing Processes (MYPP 3.5.5B)

Partners

- University of California Berkeley
 - Department of Mechanical Engineering Laboratory for Manufacturing and Sustainability
 - Transportation Sustainability Research Center
- Ballard Power Systems
- Other Industry Advisors (Altergy Systems)
- Strategic Analysis

Acknowledgment



Funding and support of this work by the U.S. Department of Energy, Fuel Cells Technologies Office is gratefully acknowledged.

Thanks also to:

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Bob Sandbank, Eurotech
Mark Miller, Coating Tech Services,
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Charleen Chang, Richest Group (Shanghai, China)
Emory De Castro, Advent Technologies
Douglas Wheeler, DJW Technology, LLC
Don Gervasio, University of Arizona
Tequila Harris, Georgia Tech University
Owen Hopkins from Entegris
Gerald DeCuollo from Treadstone
Brent Cunningham

Relevance & Goals



Total-cost-of-ownership (TCO) modeling tool for design and manufacturing of fuel cells in stationary and materials-handling systems in emerging markets

Expanded framework to include life-cycle analysis (LCA) and possible ancillary financial benefits, including:

 carbon credits, health/environmental externalities, end-of-life recycling, reduced costs for building operation

Identify system designs that meet lowest manufacturing cost and TCO goals as a function of application requirements, power capacity, and production volume

Provide capability for sensitivity analysis to key cost assumptions

BARRIERS

- High capital and installation costs with a failure to address reductions in externalized costs and renewable energy value
- Potential policy and incentive programs may not value fuel cell (FC) total benefits.

Overview: Chemistries and Applications



- Fuel cell types to be considered:
 - —Conventional, low-temp (~80°C) PEM fuel cell (LTPEM)
 - —High-temp (~180°C) PEM fuel cell (HTPEM)
 - —Solid oxide fuel cell (SOFC)

Application Space:

APPLICATION	SIZE [KW]	PRODUCTION VOLUME (UNITS/YEAR)				
		100	1000	10,000	50,000	
STATIONARY POWER /	1	C,B	C,B	C,B	C,B	
COMBINED HEAT AND POWER	10	C,B	СВ	C,B	C,B	
(C)	50	C,B	C,B	C,B	C,B	
BACKUP POWER (B)	100	С	С	С	С	
. ,	250	С	С	С	С	

Milestones / AOP FY2014



Quarter	Task Description/ Due Date	Go/No-Go Description and Due Date						
Q1 10/1/2013 12/31/2013	Detailed design plans and bill-of materials and balance-of-plant inventory for HT-PEM systems in co-generation and stationary power applications (12/31/13)	Done						
Q2 1/1/2014 3/31/2014	Direct cost model for HT-PEM systems for co-generation and stationary power applications completed (3/31/2014)	Done						
Q3 4/1/2014 6/30/2014	Literature/patent summary and functional specifications completed for SOFC systems in co-generation and stationary power (6/30/14)	In Progress						
Q4 7/1/2014 9/30/2014	7/1/2014 completed for HT- PEM systems in CHP and stationary power applications along with a							

TCO Model Structure and Key Outputs





Application/ Size
Mfg Volume/Yr
Location (mfg, op)
Prices
Policies
Fuel input
Outages/Lifetimes



Total Cost of Ownership (TCO) Model **Lifecycle Cost Model Manufacturing** Capital/installation **Cost Model LBNL** Fuel and operations **DER-CAM** Direct mfg costs Model Maintenance Indirect mfg costs (CHP) Stack replacements End of life **LBNL Life Cycle Impact Assessment Models Impact** Monetized health and GHG impacts Models/ Info



Key Outputs:

- 1) System manufacturing costs and "factory gate" prices
- 2) TCO Metrics: Levelized costs (\$/kWh), Total costs/yr
- 3) TCO including broader social costs

1 - Costing Approach



Direct Manufacturing Costs

- Capital costs
- Labor costs
- Materials costs
- Consumables
- Scrap/yield losses
- Factory costs

Global Assumptions

- Discount rate, inflation rate
- Tool lifetimes
- Costs of energy, etc.

Other Costs:

- R&D costs, G&A, sales, marketing
- Product warranty costs



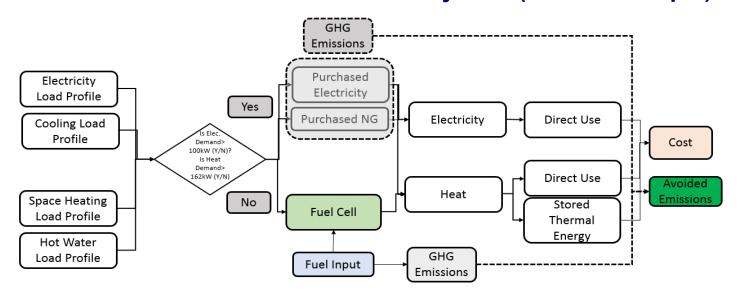


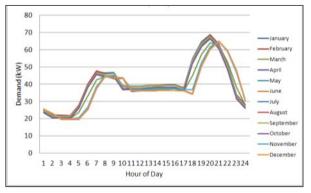
Source: Altergy Systems

2 - Fuel Cell System Life Cycle Cost (Use Phase) Modeling



Combined Heat & Power Fuel Cell System (100kW example)





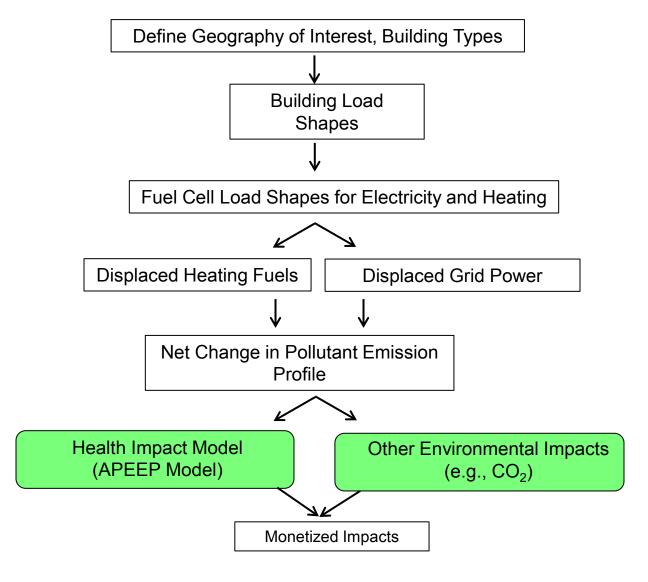
30
25
20
(W)
Pure 15
10
10
10
11
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24
Hour of Day

Daily electricity load profiles for small hotel in AZ

Daily hot water load profiles for small hotel in AZ

3 - Life-Cycle Impact Assessment for Environmental and Health Externalities – Fuel Cell CHP Systems







TECHNICAL PROGRESS: LT-PEM FC SYSTEM MANUFACTURING COST

CHP System Designs and Functional Specs



DFMA Manufacturing approaches for LT-PEM FC CHP and backup power systems

Component	Primary Approach	Reference
Membrane	Purchase Nafion®	Patent review, Industry input
CCM*	Dual Decal, slot die coating	Literature, patents, industry input
GDL*	Spray coat MPL	Literature, industry input
Bipolar Plates*	Injection molded graphite –carbon composite (and Metal Plates)	Literature, patents, industry input
Seal/Frame MEA*	Framed MEA	Patents, industry input
Stack Assembly*	Partial to fully automated	Patents, Industry input
Endplate/ Gaskets	Graphite composite/ Screen printed	Industry input, literature
Test/Burn-in	Post Assembly 3 hrs	Industry input

^{*}Full DFMA Costing analysis was performed

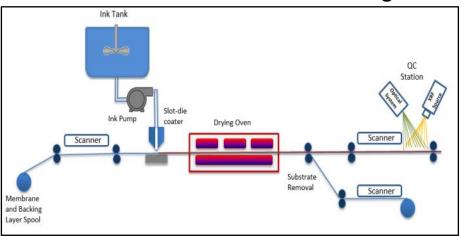
Functional specs for 100kW CHP system operating with reformate fuel, 0.5mg/cm² Pt

Parameter	Value	Unit
Gross system power	124	kW
Net system power	100	kW
Electrical output	480V AC	Volts AC or DC
Waste heat grade	65	Temp. °C
Fuel utilization	80-95	%
Avg. System Net	32	% LHV
Electrical efficiency		
Thermal efficiency	51	% LHV
Total efficiency	83	Elect.+thermal (%)
Stack power	9.5	kW
Total plate area	360	cm ²
CCM coated area	232	cm ²
Single cell active area	198	cm ²
Cell amps	111	Α
Current density	0.56	A/cm ²
Reference voltage	0.7	V
Power density	0.392	W/cm ²
Single cell power	78	W
Cells per stack	122	Cells
Stacks per system	13	Stacks

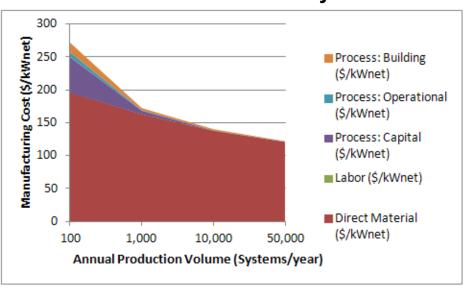
Manufacturing Cost Model – CCM, Metal Plates



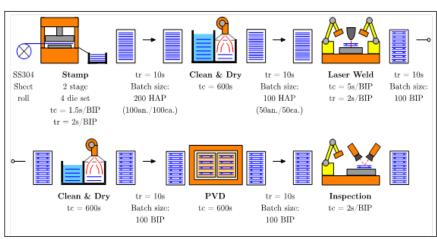
CCM Process Flow-Cathode Coating Line



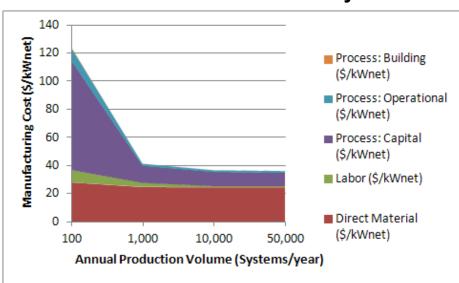
CCM Cost Plot - 100kW System



Metal Plate Process Flow

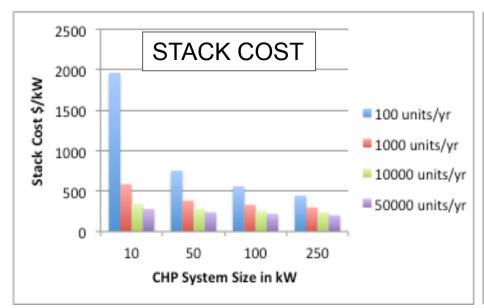


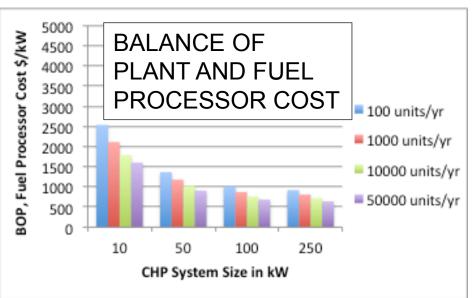
Plates Cost Plot - 100kW System

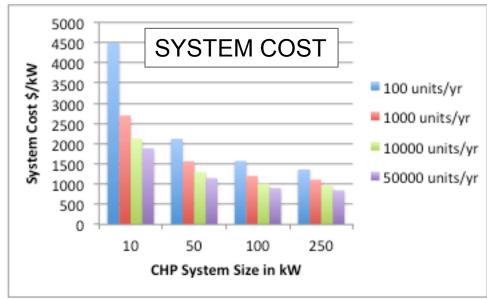


Summary of Cost vs. Volume for CHP System Sizes of 10, 50, 100, and 250 kW



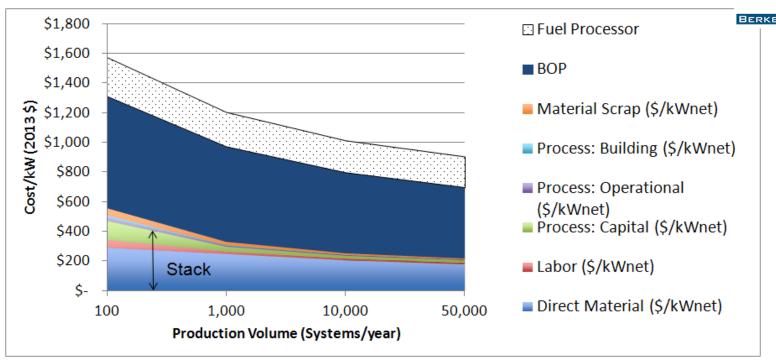


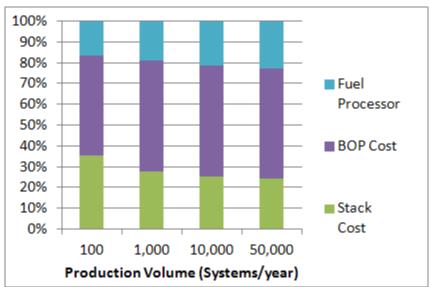


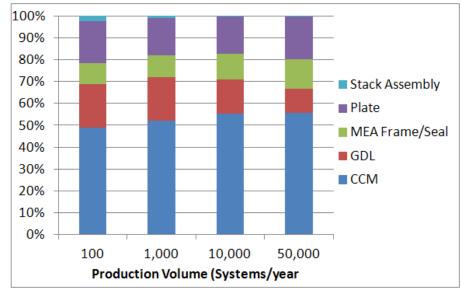


100kW CHP System Cost vs. Volume



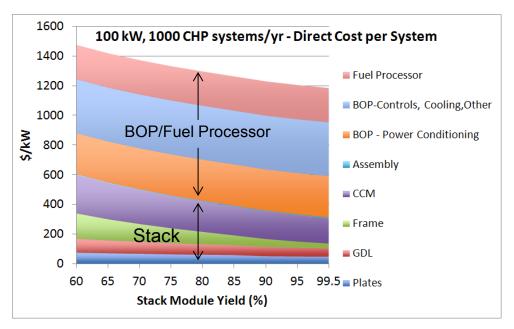






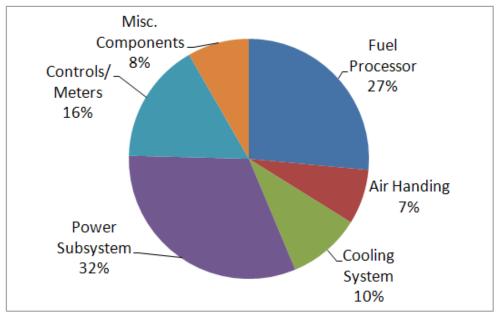
100kW CHP System Cost vs. Yield at Fixed Volume





BOP/Fuel Processor are dominant fraction of system costs

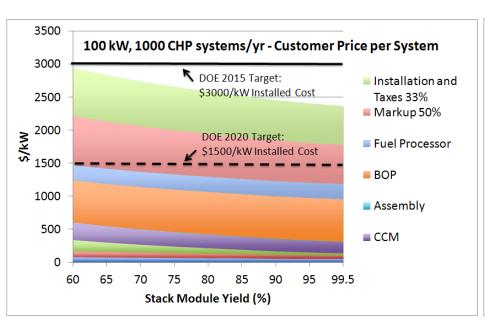
Stack costs are a strong function of stack module yield

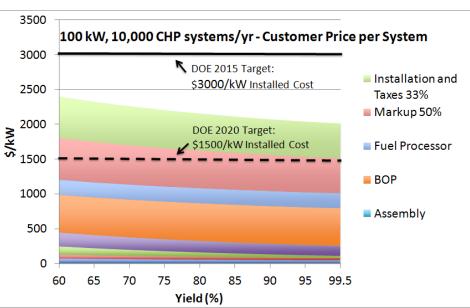


Non-Stack component cost reduction opportunities in power subsystem and fuel processor

Installed Cost for 100kW CHP Systems



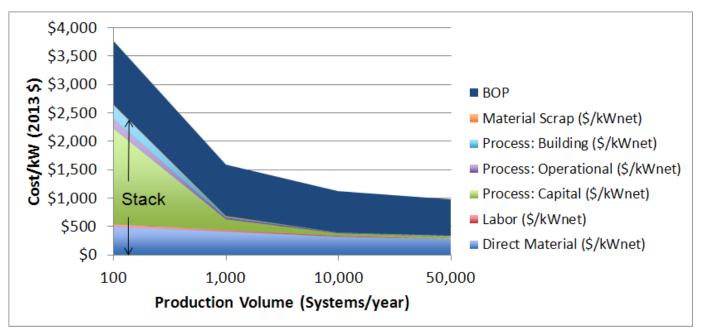


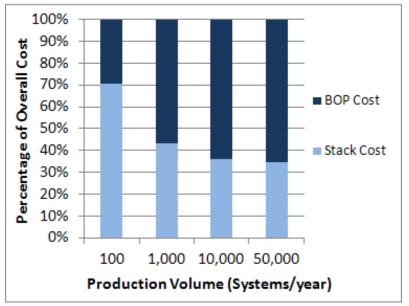


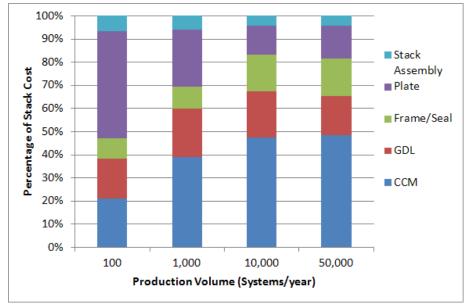
100kW CHP can meet 2015 DOE target at 1,000 - 10,000 systems/year, but further cost reduction needed to meet 2020 target

10kW Backup Power System Cost vs. Volume

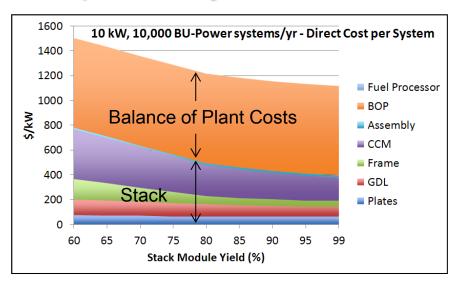




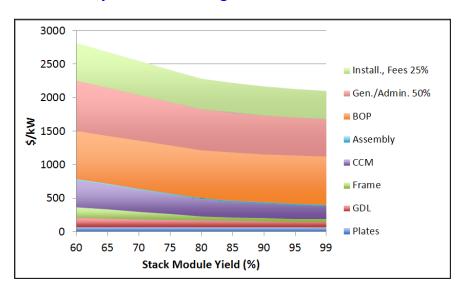




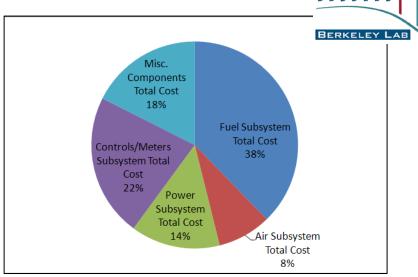
Backup Power System Cost Modeling at Fixed Volume



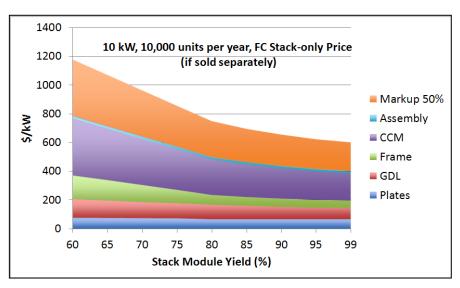
Stack costs are a strong function of stack module yield; Balance of plant costs are greater than FC Stack costs



10kW Backup Power system total installed cost just under \$2200/kW at 90% stack module yield



BOP cost analysis highlights cost reduction opportunities in fuel subsystem and controls/meters



10kW Stack-only price is \$650/kW at 90% stack module yield



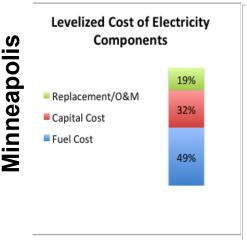
TECHNICAL PROGRESS: TOTAL COST OF ELECTRICITY

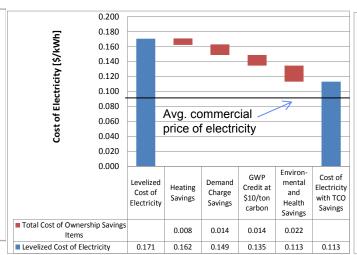
Total Cost of Ownership Modeling Example 100kW CHP System, Small Hotel

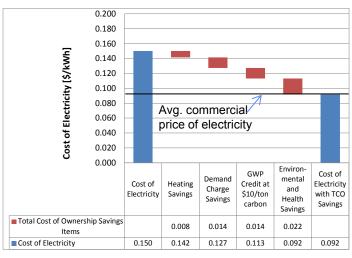


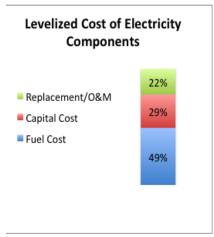


\$1,500/kW installed cost

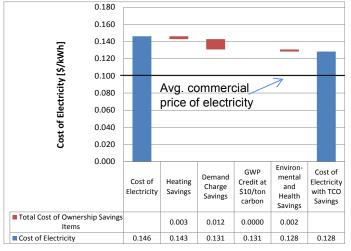


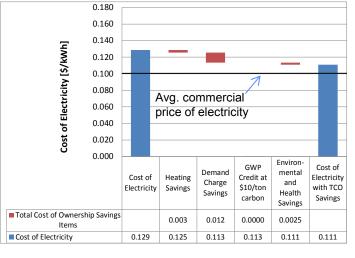






Phoenix

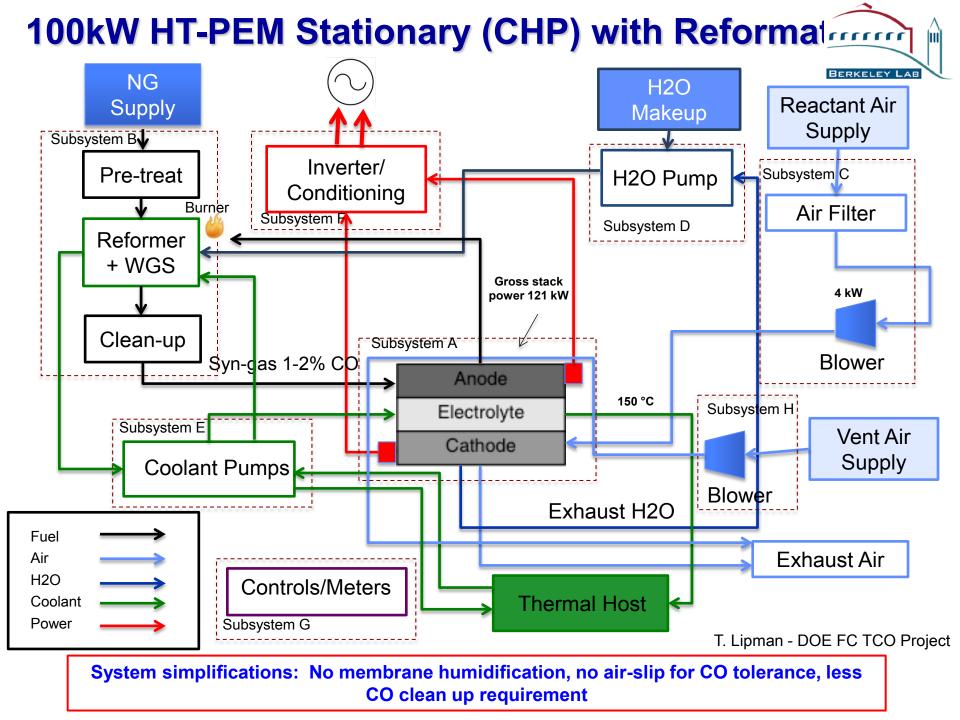




Externality valuation (GHG, health) contributes up to 20-24% savings in "total cost of electricity" in regions with "dirty electricity" such as upper Midwest Up to 39% overall reduction in total cost of electricity including all TCO items



TECHNICAL PROGRESS: HT-PEM FC SYSTEM MANUFACTURING COSTS



CHP Functional Specifications

100kW CHP system operating with reformate fuel

100 kW Size		Best. Ests.	
	Unique Properties:		<u>Units:</u>
<u>System</u>	Gross system power	121	kW
	Net system power	100	kW (AC)
	Physical size	2.9x4.2x3.6	meter x meter x meter
	Physical weight	14080	kg
	Electrical output	480V AC	Volts AC or DC
	DC/AC inverter effic.	93%	%
	Peak ramp rate	0.372	kW/sec - size dep
	Waste heat grade	150	Temp. °C
	Reformer efficiency	75%	%
	Fuel utilization % (first pass)	80%	%
	Fuel utilization % (overall)	95%	%
	Fuel input power (LHV)	335	kW
	Stack voltage effic.	51%	% LHV
	Gross system electr. effic.	36%	% LHV
	Avg. system net electr. effic.	30%	% LHV
	Thermal efficiency	53%	% LHV
	Total efficiency	83%	Elect.+thermal (%)
<u>Stack</u>	stack power	8.08	kW
_	total plate area	720	cm^2
	CCM coated area	464	cm^2
	single cell active area	422	cm^2
	gross cell inactive area	41	%
	cell amps	106	A
	current density	0.25	A/cm^2
	reference voltage	0.625	V
	power density	0.157	W/cm^2
	single cell power	66	W
	cells per stack	122	cells
	percent active cells	100	%
	stacks per system	15	stacks
Addt'l Parasitics	Compressor/blower	4	kW
	Other paras. loads	9.72	kW
	Parasitic loss	13.72	kW



DFMA Manufacturing Approaches for HT-PEM CHP Applications

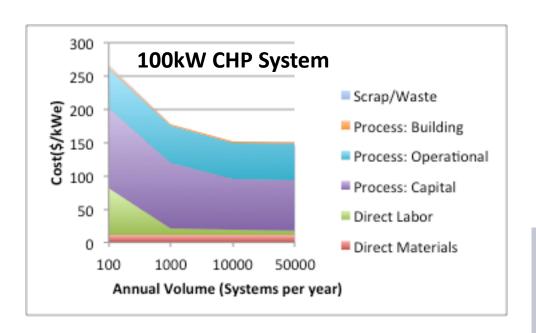


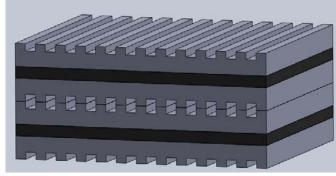
			BERKELEY LAB
Component	Primary Approach	Reference	LT-PEM Approach
Membrane*	PBI-PPA process	Patent review, Industry/University inputs	Purchase Nafion®
Catalyst Layer*	Gas Diffusion Electrode (GDE) with slot die coating Catalyst loading 0.7mg/cm ² Pt	Literature, industry input	CCM with Dual Decal, slot die coating – Catalyst loading 0.5mg/cm²
GDL*	Carbon paper Spray coat MPL	Literature, industry input	Carbon Paper Spray coat MPL
Bipolar Plates*	Compression molded graphite/resin plates with separator layer	Patent review, Industry/University inputs	Injection molded graphite –carbon composite
Seal/Frame MEA*	Framed MEA	Patents, industry input	Framed MEA
Stack Assembly*	Partial to fully automated	Patents, Industry input	Partial to fully automated
Endplate/ Gaskets	Graphite composite/ Screen printed	Industry input, literature	Graphite composite/ Screen printed
Test/Burn-in	Post Assembly 3 hrs	Industry input	Post Assembly 3hrs

Key modules: Membrane, Plates; Others similar to LT-PEM case.

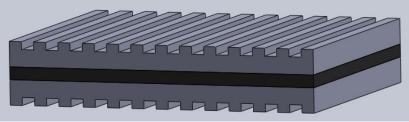
Plates with Separator Layer

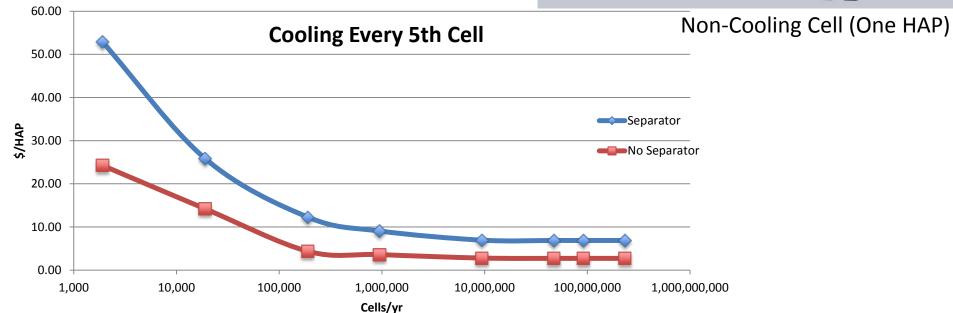






Cooling Cell (Two HAP)

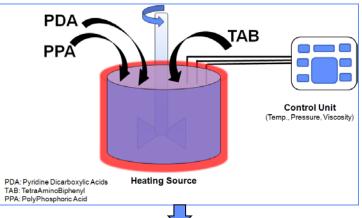




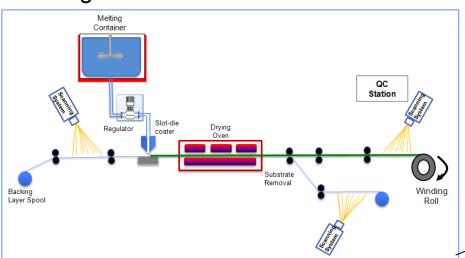
PBI Membrane Process Flow



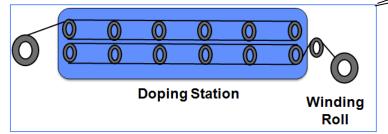
Mixing/heating monomers

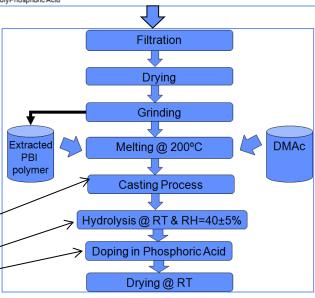


Casting



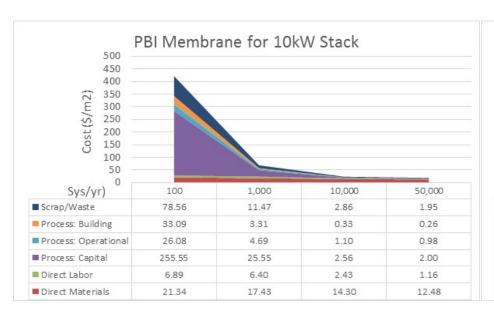
Hydrolysis and Doping

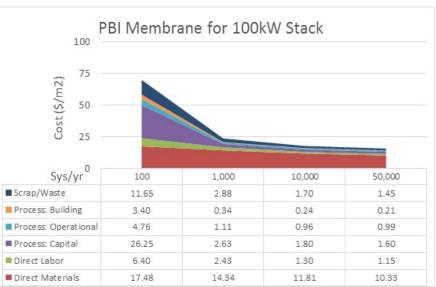




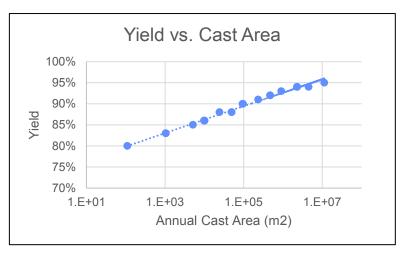
PBI Membrane- Cost Breakdown





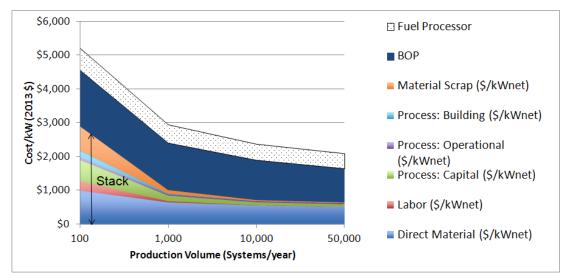


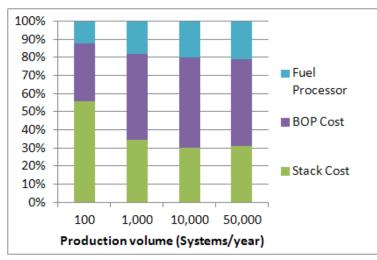
Materials	Price
Isophthalic acid	\$103 for 5kg
Terephthalic acid	\$377 for 10kg
3,3',4,4'-Tetraaminobiphenyl (TAB)	\$380 for100 g
Polyphosphoric acid (115%)	\$60 for1 kg
Ammonium Hydoroxide	\$253.5 for 6 ltrs
N,N-DiMethylAcetamide (DMAc)	\$62.2 for 2 ltrs



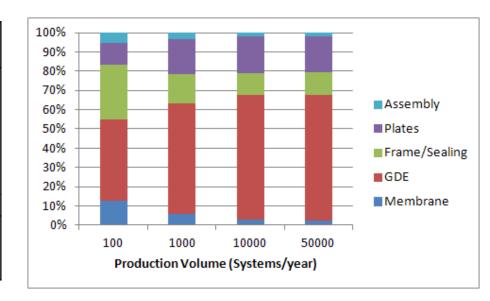
Preliminary Cost for 10kW HT-PEM CHP System





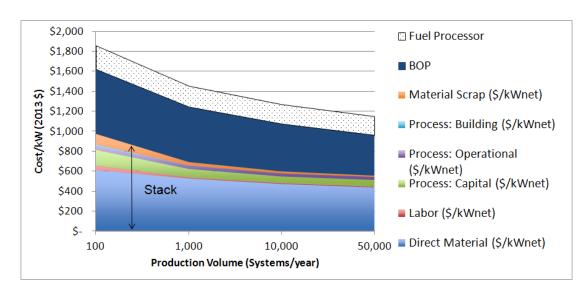


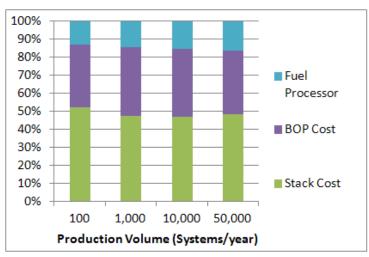
Power (kW)	10 1			10	10			10	
Systems/Yr		100		1000		10000		50000	
Direct Materials (\$/kW)	\$	990	\$	640	\$	552	\$	511	
Direct Labor	\$	277	\$	45	\$	10	\$	9	
Process: Capital	\$	632	\$	158	\$	83	\$	67	
Process: Operational	\$	88	\$	45	\$	36	\$	35	
Process: Building	\$	190	\$	18	\$	3	\$	2	
Scrap/Waste	\$	722	\$	106	\$	32	\$	22	
Final Stack Cost (\$/kW)	\$	2,898	\$	1,013	\$	717	\$	646	
BOP_non FP	\$	1,664	\$	1,395	\$	1,185	\$	1,006	
BOP_FP	\$	653	\$	542	\$	475	\$	444	
Total Cost (\$/kW)	\$	5,215	\$	2,950	\$	2,377	\$	2,096	



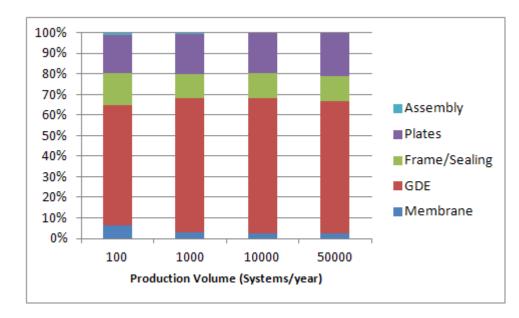
Preliminary Cost for 100kW HT-PEM CHP System







Power (kW)	100	100		100		100	
Ssystems/Yr	100		1000	1	.0000	50000	
Direct Materials (\$/kW)	\$ 613	\$	528	\$	474	\$	440
Direct Labor	\$ 41	\$	9	\$	7	\$	7
Process: Capital	\$ 158	\$	83	\$	64	\$	62
Process: Operational	\$ 44	\$	36	\$	34	\$	34
Process: Building	\$ 11	\$	3	\$	1	\$	1
Scrap/Waste	\$ 106	\$	32	\$	18	\$	11
Final Stack Cost (\$/kW)	\$ 973	\$	691	\$	598	\$	555
BOP_non FP	\$ 648	\$	555	\$	479	\$	410
BOP_FP	\$ 236	\$	208	\$	194	\$	186
Total Cost (\$/kW)	\$ 1,857	\$	1,454	\$	1,271	\$	1,151



Responses to 2013 AMR Reviewer Comments



1. How does this fit in with other DOE cost analysis work?

Response: This work is part of a complimentary portfolio of DOE analysis projects. Other projects have focused on different applications (e.g., MHE) and other technologies (SOFC). This project also expands the direct cost modeling approach to include life-cycle costing and ancillary financial benefits (GHG credits, health and environmental impacts).

2. More vendor/OEM input and feedback is needed for costing validation.

Response: Extensive vendor/OEM feedback was obtained for stack module equipment and process parameters (e.g., roll-to-roll processing, plate processing), balance of plant components (vendor quotes), functional specifications (Ballard Power Systems), and overall costing (Ballard Power Systems and Altergy Systems). Further feedback and OEM input is being sought from international companies such as Panasonic Corporation and Nedstack Fuel Cell Technology B.V. for smaller power CHP systems and backup power systems, respectively.

2. What are cost reduction opportunities beyond volume scaling? Why does balance of plant appear so large and what are cost reduction opportunities there?

Response: This work has shown the importance and sensitivity of stack module yield on stack costs (e.g., the need for improved defect metrology and inline to end of line defect characterization) and the importance of balance of plant cost reduction for overall system cost reduction (e.g., power conditioning, potential cost reduction from design and integration). We have identified power conditioning as a key area for CHP systems. There are many parts in the balance of plant contributing to the overall cost, and increased parts-integration is a potential cost reduction opportunity. For back-up power and smaller size CHP systems, we are revising the BOP components, integration, and resultant cost in consultation with industry advisors.

Collaborations



Partners

University of California Berkeley

Laboratory for Manufacturing and Sustainability, Dept. of Mechanical Engineering:

Manufacturing process analysis, DFMA analysis

Transportation Sustainability Research Center and DOE Pacific Region Clean Energy Application Center:

- System and BOP design, functional specs, BOM definition, parametric relationships
- CHP applications and functional requirements

Ballard Power Systems

Consultation on fuel cell system design and manufacturing processes

Strategic Analysis:

Fuel processor systems and DFMA costing

Other Collaborators

Altergy Systems: Consultation on backup power system

Panasonic Corporation: will review of low power CHP systems

Remaining Challenges & Future Plans



Challenges

- Lack of HT-PEM vendors and OEM contacts have started discussion with Advent Technologies, PAFC contacts
- Refined estimate of lower power CHP and backup power balance of plant engagement planned w/ Panasonic, Nedstack
- SOFC vendor/OEM industry advisors industry contacts being developed
- Lack of data for system availability will add as a sensitivity factor to LCC model, HT-PEM pilot data

Plans

- Currently refining DFMA cost model for High Temperature PEM CHP and developing LCC/TCO model
 - Membranes; High temperature, long lifetime plates
 - LCC with absorption cooling option
- Solid oxide fuel cell functional spec definition, system design, and DFMA in next few months
- Also automating LT-PEM TCO model for user enabled interface in Analytica

Project Summary



Relevance: Provide more comprehensive cost analysis for stationary and materials handling fuel cell systems in emerging markets including ancillary financial benefits.

Approach: Design for manufacturing and assembly (DFMA) analysis cost model and integrated lifecycle cost analysis (LCA) impacts including life cycle costs, carbon credits, and health and environmental benefits

Technical Accomplishments and Progress: Total cost of ownership model for LT-PEM CHP systems (manufacturing cost model, LCC model and externality valuation); Direct cost model for HT-PEM CHP system

Collaboration: Partnerships with UC-Berkeley manufacturing analysis and transportation sustainability research groups and Ballard Power Systems. Collaboration with Strategic Analysis and Altergy Systems

Proposed Next-Year Research: Total cost of ownership model for HT-PEM systems and Manufacturing Cost model for SOFC CHP and power-only system

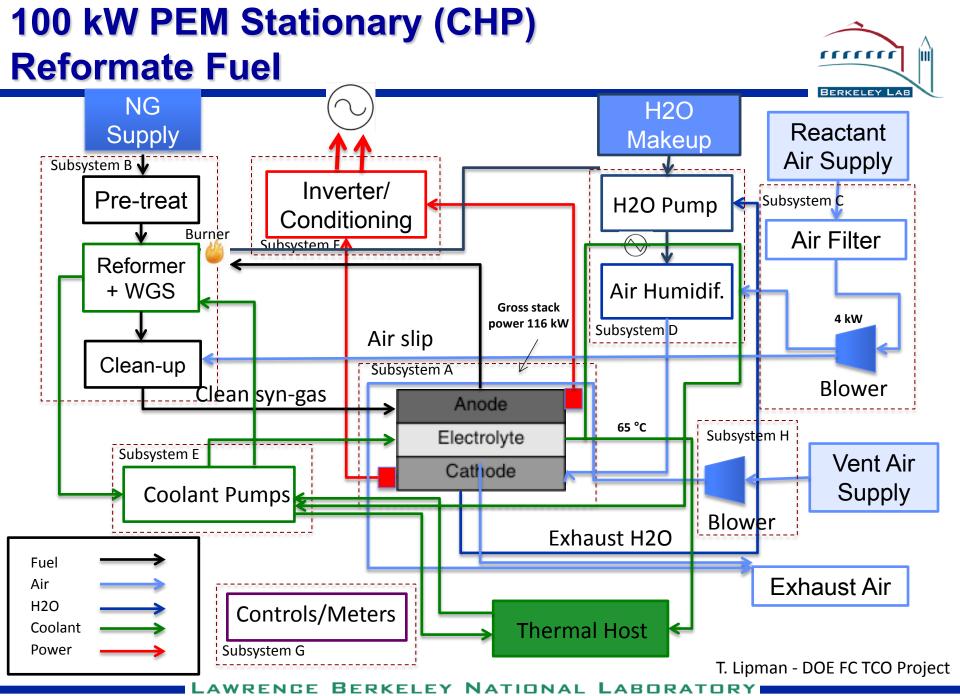
Max Wei 510-486-5220 mwei@lbl.gov Tom McKone 510-486-6163 TEMcKone@lbl.gov



Thank you mwei@lbl.gov

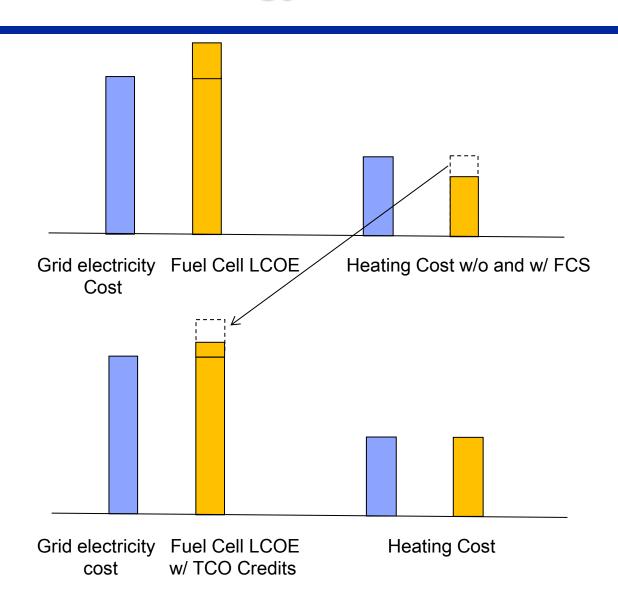


Technical Back-Up Slides



Cost of Energy Service with FC CHP



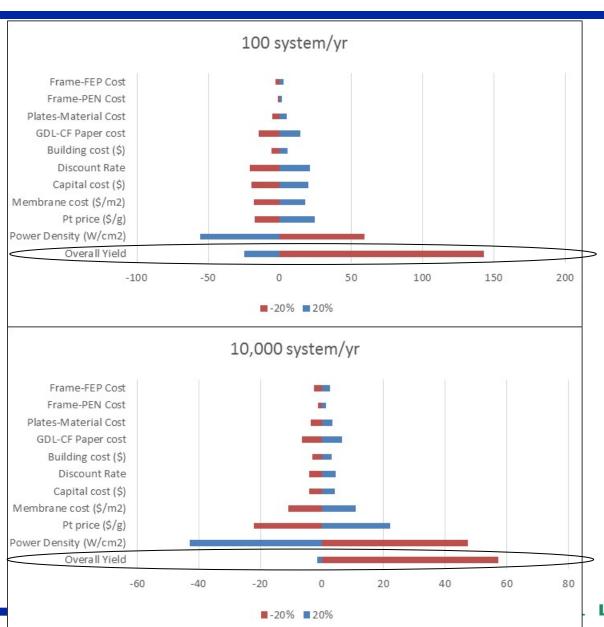


Take heat savings as a credit to FC cost of electricity, and similarly with other TCO credits.

Then compare Fuel Cell "Levelized Cost of Electricity With TCO credits" to Grid Electricity cost (\$/kWh)

Stack Manufacturing Cost Sensitivity (\$/ kW)

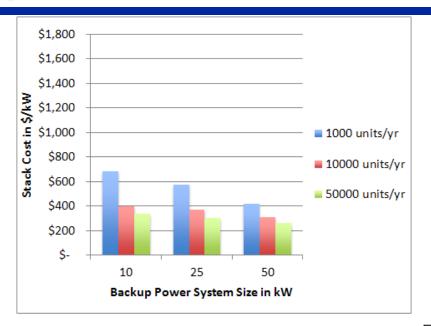


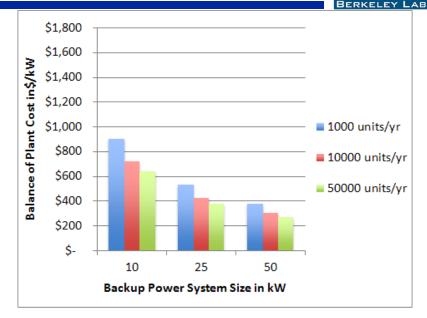


Yield (module level) dominates followed by power density and Pt price

LABORATORY

Direct Cost vs. Volume for FC Backup Power Systems





rrrrrr

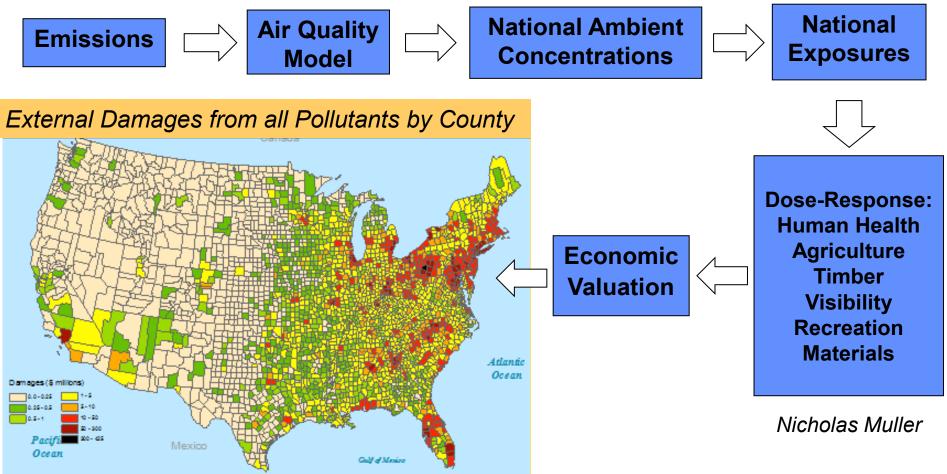
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\$1,800					
\$1,600				_	
≥ ^{\$1,400}	_			_	-
\$1,400 \$1,200				_	
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\$600 \$400				-	
<i>ຮ</i> ້ _{\$400}				_ = 50000 units/yr	
\$200		_	_	_	
\$-					_
	10	25	50		
	Backup P	ower System	Size in kW		Y
					-

	kWe	1000 nits/yr	10000 units/yr				10000 to 50000	10,000 to 100,000
						units	units	units
								extrap.
	10	\$ 683	\$ 402	\$	338	41%	16%	29%
STACK	25	\$ 573	\$ 369	\$	303	36%	18%	32%
	50	\$ 417	\$ 311	\$	260	25%	17%	30%
	10	\$ 902	\$ 720	\$	639	20%	11%	21%
BOP	25	\$ 532	\$ 425	\$	377	20%	11%	21%
	50	\$ 380	\$ 303	\$	269	20%	11%	21%
	10	\$ 1,585	\$ 1,122	\$	977	29%	13%	24%
SYSTEM	25	\$ 1,105	\$ 794	\$	680	28%	14%	27%
	50	\$ 797	\$ 614	\$	529	23%	14%	26%

Note: Stack costs in \$/kWe based on bottom-up direct manufacturing cost analysis; BOP costs are purchased components

Air Pollution Emissions Experiments and Policy Analysis Model (APEEP)





- Focus on ambient concentrations of PM_{2.5} and O₃ (dominant health and environmental externalities)
- Model adopted by U.S. National Academy of Sciences for "Hidden Cost of Energy" study (2010)